SRI	FOR SVNCAS	PURIFICATION	UNIT OF LATE.	2 · RHFI	REPLIES TO PL	F-RID (DIFFRIES DATE	TD 07-02-20	125

SI.No.	Part / Volume	Page	Clause	Subject	Exiting Provision	Bidders Queries dated 07-02-25	BHEL Clarification	Gaseous Emission: Stack gas Emission Limits:	
		No.	No.	,				S. No. Source Suspended S	6O _X NO _X CO /Nm³) (mg/Nm³) (mg/Nm³
	TECHNICAL CONDITIONS OF CONTRACT PY 54037 Rev1	Sheet 10	5.9	Gaseous Emission	No H2S emission limit available	Emission limit for H2S is essential to properly design the thermal incinerator. BHEL to provide the latest applicable norms, where H2S emission limit is indicated, considering that the failure to meet this guarantee is considered a breach of contract.	Bidder shall guarantee the limits of pre-treated liquid effluents at the Battery Limit, gaseous emission to the atmosphere and noise levels (as specified) as per the relevant existing and latest norms of CPCB, PESO and other applicable stringent environmental norms of CPCB/state pollution control board. The determination of the ability of Purification Plant to meet these guarantees will be made during the thirty days' guarantee test or at any other time under similar conditions prior to the Preliminary Acceptance of the Process Plant/ Units. In the event guaranteed pollution level are not fulfilled during the 30days' guarantee test it shall be breach of contract, requiring corrective action by bidder irrespective of the cost involved.	Gas Matter (mg/Nm³)	<50 <250 <100 <100 orms of stringent CPCB/state p
	ANNEXURE 5	-	1.0	Specification of Hydrogen Sulfide (H2S)	H2S Fraction composition for Design Case	Preliminary composition of H2S fraction provided at Annexure 5 indicates a normal H2S content of 34.08 % vol. A minimum H2S content of 25% vol is also indicated in Annexure 5. Since the minimum H2S content is the design case for the SRU, BHEL to confirm if the design case shall be defined as follows: - H2S content of 25% vol, - all other compounds: proportionally increased to normalize the composition up to 100%. - Total H2S Fraction flow rate: increased in order to reach a sulphur production of 8.8 TPD. Or alternatively, BHEL to confirm that H2S min. 25% value is discarded and the H2S fraction complete composition shall be considered.	The preliminary data available is provided to bidders. Bidders to size considering the stringent case, however, same cane be reviewed during detailed engineering stage.	Storage pressure =	R. Fifteen day's p m² (To be specif Atmospheric OWNER
	TECHNICAL CONDITIONS OF CONTRACT PY 54037 Rev1	Sheet 3	1.2	SRU Capacity	8 TPD +_ 30%	According to BHEL reply, the SRU normal capacity is approximately 8 TPD (7.8 TPD according to H2S fraction composition at Annexure S) and additional 10% design margin has to be considered; the turndown capacity is 50% of the normal one. Therefore, the sentence of the capacity variation of ±30% can be disregarded during bidding phase. BHEL to confirm.	Yes, Bidder's understanding is correct.	Storage for solid Sulphur will be a The open pit shall have two comp truck loading arrangement. The Flooring &dyke wall should be ant	in open pit for min. 15 partments along with open pit should hav
	TECHNICAL CONDITIONS OF CONTRACT PY 54037 Rev1	Sheet 4	3.5	Sulphur Recovery Unit (SRU) & Sulphur Storage	Liquid / Solid Sulphur Facilities	Bidder understands that liquid sulphur shall be normally delivered in liquid state to the storage area. BHEL to define/confirm the following: a) Define the hold-up time of liquid sulphur in the sulphur pit. b) Confirm that sulphur storage area/facilities are excluded from Licensor scope of work. c) Confirm that no solidification unit is required. d) Confirm that no loading arm shall be foreseen. e) Define the battery limit pressure of the liquid sulphur from the Sulphur Pit Pumps.	Bidder to carry out the BEDP to meet the specifications listed under clause no. 5.8 of the tender specifications. a) Hold time shall be as per the ttachhed excerpts of specification. b) Sulphur storage area shall be designed by the main by the Engg. sub-contractor, however, all the necessary input data shall be furnished by the process licensor. c) As per the attached excerpts of specification soldification unit is not envisaged except the sulphur pit. d) Truck loading facility is envisaged as per the specifications. e) Bidder to finalise during detailed engineering, however, for preliminary design please refer to the plot plan which indicates the location of SRU unit and sulphur pit.	Transfer of liquid Sulphur from gassifier) located at LSTK B.L. to LSTK CONTRACTOR. One Tanl sulphur to be provided by LSTK CONTRACTION. H2S Fraction Given figures are the result of the	above mentioned stock Truck lorry loading Contractor.
	TECHNICAL CONDITIONS OF CONTRACT PY 54037 Rev1	Sheet 8	5.5	Minimum facilities	Number of Claus Trains	At mentioned clause it is indicated that "Acid gas Knock out drum and Sour gas knock out drum can be shared after which the acid gas can be split for single train of SRU." Bidder is considering a single Claus Train. BHEL to confirm.	Yes, Bidder's understanding is correct.	H2S Fraction mole% Nm ³ /h H2 0,19 N2 19,63 1 CO 0,01	1 1224 0
	TECHNICAL CONDITIONS OF CONTRACT PY 54037 Rev1	Sheet 15/16	12.13	Works cost (Consumption of Raw material & Utilities)	Fuel Gas Availability	Fuel Gas is not indicated among Utilities. BHEL to specifity type, composition and conditions of Fuel Gas, available at SRU battery limits, both in normal operation and at SRU start-up.	Cuality	H2S 34,04 2	0 0 0 778 214 11 1 0 0
	TECHNICAL CONDITIONS OF CONTRACT PY 54037 Rev1	Sheet 15/16	12.13	Works cost (Consumption of Raw material & Utilities)	Oxygen Availability	Oxygen is not indicated among Utilities. BHEL to specify composition and conditions of gaseous Oxygen, if available at SRU battery limits.	Bidder to inform the reuquirements and BHEL shall expedite the same form BCGCL.		530
	TECHNICAL CONDITIONS OF CONTRACT PY 54037 Rev1	Sheet 15/16	12.13	Works cost (Consumption of Raw material & Utilities)	Clean Syngas Availability	Hydrogen rich stream is required in SRU TGT section. BHEL to specify composition and conditions of Syngas available at SRU battery limits.	Bidder to refer to the attached snapshot in this sheet. Kindly note that the composition is based on the preliminary design and will be subject to changes during the detailed engineering phase.	Return Header Pressure, kg/cm²g (Min/ Nor/ Max) Mechanical Design Pressure, kg/cm²g	LSTK contractor to decide LSTK contractor to decide
	TECHNICAL CONDITIONS OF CONTRACT PY 54037 Rev1	Sheet 15/16	12.13	Works cost (Consumption of Raw material & Utilities)	Cooling Water Availability	Cooling Water is not indicated among Utilities. BHEL to specifity characteristics and conditions of Cooling Water, if available at SRU battery limits.	Bidder to refer to the attached snapshot in this sheet.	Mechanical Design Temperature, C	By LSTK Contractor 60 10 °C max.
	TECHNICAL CONDITIONS OF CONTRACT PY 54037 Rev1	Sheet 15/16	12.13	Works cost (Consumption of Raw material & Utilities)	Utilities Conditions	BHEL to specify characteristics and conditions at SRU BL of the following imported utilities: Low Pressure Nitrogen, Demi Water, BFW.	Nitrogen (Utility/Process) Utility Process Piressure, kg/cm²g (Min/Nor/Design) 6.0/8.0/9.0 35 Temperature Ambient ≤100 N ₂ Vol ½, min 99.99% 99.99% O ₂ , Vol ppm <10	Chlorides, mg/l Sulphates, mg/l	100% (max.) 5 7-8.5 100
	TECHNICAL CONDITIONS OF CONTRACT PY 54037 Rev1	Sheet 15/16	12.13	Works cost (Consumption of Raw material & Utilities)	Utilities Conditions	BHEL to specify conditions at SRU BL of the following exported utilities: Low Pressure Steam Condensate.	L.P Steam	Manganese, mg/l	15 000 Traces Traces
	TECHNICAL CONDITIONS OF CONTRACT PY 54037 Rev1	Sheet 13	12.4	Pollution Level	Liquid Effluent	BHEL to confirm if boilers blow down can be discharged to sewer after cooling.	Biddder to indicate the Qlty. & Qty. , BHEL will take care of the reqquired treatment.	Calcium Hardness, mg/l as CaCO ₃ 5	500 750

S. No.	Source	Particulate Matter (mg/Nm³)	SO _x (mg/Nm³)	NO _x (mg/Nm³)	CO (mg/Nm³)	
	Gas					l
1.	Purification	s 5	<50	<250	<100	l
	section					l

vith proper concrete dyke) shall be

oroduction

ified by LSTK CONTRACTOR)

ACTOR at B.L. of Storage.

15 days storage. h ramp provision for pay loader and ave proper water drainage system. eight wil∥ be min. 2 meter.

age (i.e. Sulphur pit including de-torage shall be the responsibility of g bay with covered shed for liquid

	TECHNICAL CONDITIONS OF CONTRACT PY 54037 Rev1	Sheet 13	12.4	Pollution Level	Sour Water	If liquid effluent quality as per table in para, 12.4 Pollution level is to followed, then	Bidder to follow the sour water reuquirements indicated in the table of clause 12.4 and accordingly take care of the design of the process & equipment.	
	TECHNICAL CONDITIONS OF CONTRACT PY 54037 Rev1	-	-	-	Site Conditions	BHEL to specify site Climatic Data (temperature, humidity, etc.) required for the unit design.	Bidder to refer to the attached snapshot in this sheet.	Ì

CLIMATIC DATA:

Wind:

Wind Load Design: as defined in IS: 875 Part 3

Parameters	Temperature, °C	Remarks
Dry bulb (Summer)	Max: 47.19 ° Min: 10.99 °	
Dry bulb (Winter)	Max: 37.84 ° Min: 10.17 °	
Average Temperature	26.2 •	
wet bulb	-	
Max for Mechanical / Civil / Structural	35 °C (HOLD)	
Minimum for winterization (Average)	-	

7.2.1 Atmospheric Air Composition:

1.2.1 Autiospheric All Co	mposition.
SOx	9.18
NOx	27.70
NH ₃	-
SPM ₁₀	44.15
HC (methane)	-
HC (non methane)	-
CO	-
VOC	-

NOTE: Bidder to take correction factors and worst atmospheric condition on above.

Relative Humidity	RH%
Relative Humidity,Minimum	21.79%
Relative Humidity,Maximum	99.5%
Relative Humidity Average	74%

Rainfall	Value
Annual	1534.5 mm
Design rainfall (per hour)	-

Note: - Civil philosophy is to be referred

Barometric Pressure:							
Barometric Pressure	Value						
Average	904.45						

Seismic Design Code: Refer Section-5.5 (Design Philosophy – Civil & Structural Works) Part II-Technical.

Plant Elevation:
The final plant elevation shall be established in consultation with owner / consultant based on overall project requirement.

return cooling water header within his battery limit.

Demineralised Water			
Pressure @ B/L, kg/cm ² g (Min/ Nor/ Max)	0/ 5.5/ 6.0		
Temperature, °C (Normal)	Α	mbient/40 (max)	
Mech. Design Pressure, kg/cm ² g	10)	
Mech. Design Temperature, °C	70)	
рН	6.	5-8.5	
Total Hardness, ppm wt.	ero		
Total Dissolved Solids, ppm wt (max.)	0.	.1	
Conductivity at 20 deg C, micro mho/cm (max.)	<(<0.2	
M Alkanity as CaCO ₃ , ppm wt.	N	il	
Chlorides, ppm wt.	N	il	
Iron as Fe, ppm wt. (max.)	0.01		
Silica as SiO ₂ , ppm wt. (max.)	0.02		
Oil, ppm wt.	Nil		
Sodium as Na, ppm wt. (max.)		< 0.1	