

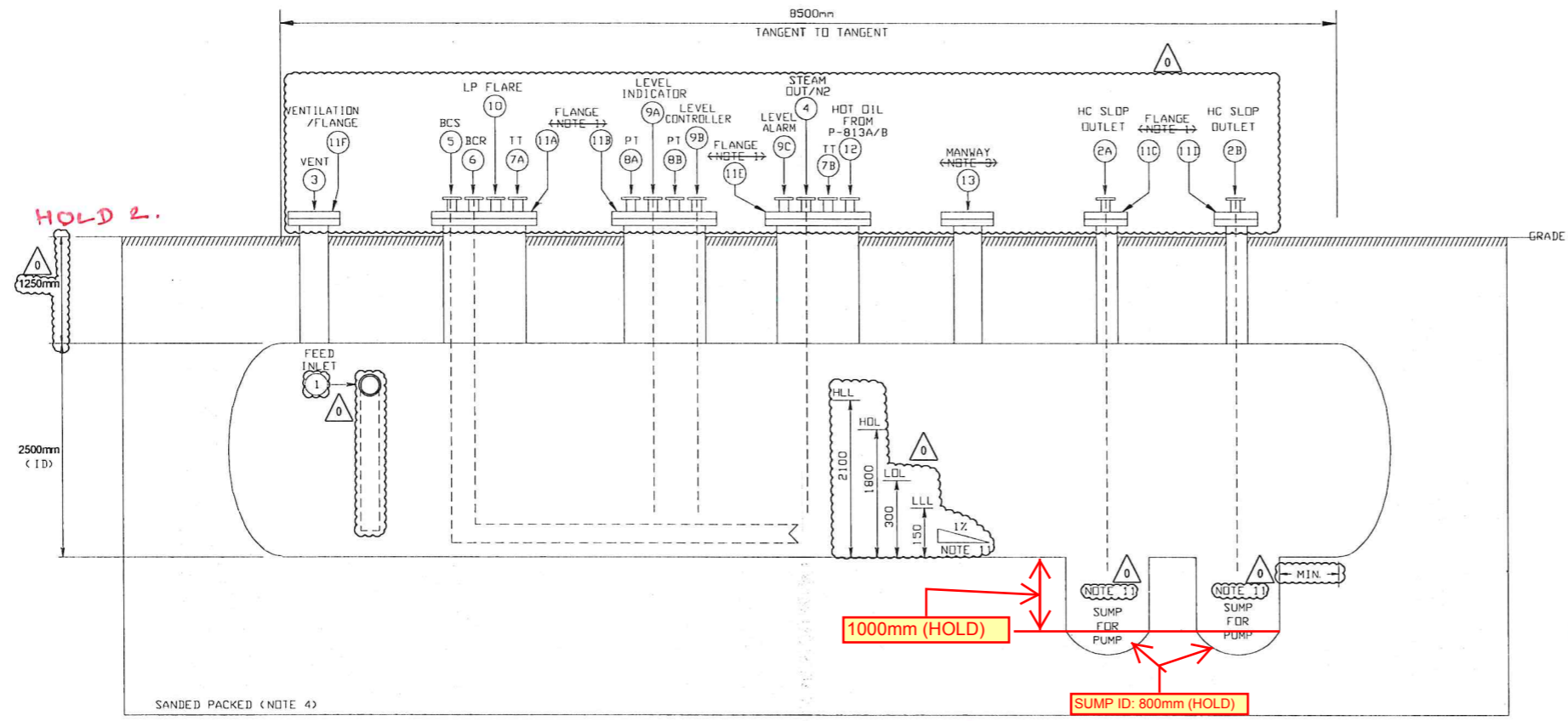


Shell- 26 Thk  
 Typical- Head : 2:1 Ellipsoidal Head Thickness : 22 mm Min.  
 ALL TOP NOZZLES TYP. PROJECTION FROM VESSEL TOP = 3000 mm (hold)  
 Steam Coil- 3 inch Sch160, 22 mtr (Hold)  
 FABRICATED WEIGHT = 34000 kg  
 PWHT & Impact test requirement : As per code/specification/data sheet  
 Note: Above Indicated Weights and Thicknesses for pressure parts and non-pressure parts are minimum to be followed and shall not form the basis for quotation. supplier shall check the thickness to satisfy the requirement of codes ,standards and requisition and guarantee them on strength.

VENDOR TO CONSIDER 5TONS(HOLD) LOAD FOR PUMP FOR PUMP HOSING NOZZLE, THE FINAL LOAD TO BE INFORMED DURING DETAILS ENGINEERING.

NOTES  
 11. VESSEL SHALL BE SLOPED TOWARDS THE SUMP. SUMP SHALL BE LOCATED TOWARDS SLOPING END OF VESSEL.

NOTES  
 1. (DBE) MECHANICAL TO DESIGN ALL FLANGES.  
 2. VENT & STEAM OUT NOZZLE SIZES SHOWN ARE BASED ON (DBE) MECHANICAL TO DESIGN ALL FLANGES.  
 3. MANWAY SIZE IS RECOMMENDED MINIMUM. LOCATION TO BE DETERMINED BY DBE. (DBE) MECHANICAL TO DESIGN ALL FLANGES.  
 4. THIS DRUM TO BE LOCATED INSIDE RCC WITH SAND PACKED BY VIBRO COMPRESSION WITH LEAN CONCRETE ON TOP. RELATIVE LOCATION OF DRUM V.R.T. GROUND LEVEL ETC. TO BE FINALISED BY GENERAL CIVIL DURING DETAIL ENGINEERING.  
 5. COIL AND FOR BCS AND BCO COIL TO BE BELOW THE LOW LIQUID LEVEL.  
 6. STEAM OUT CONDITIONS ARE 0.5 kg/cm<sup>2</sup>g AND 170°C.  
 7. DRUM TO HAVE CATHODIC PROTECTION.  
 8. VENTILATION NOZZLE IS TO BE LOCATED TOWARDS THE END OPPOSITE TO THE MANWAY. VENT NOZZLE SHALL BE WELDED TO THE VENTILATION NOZZLE BLIND FLANGE.  
 9. TRIM B1A  
 10. MDMT: 12.5°C



1000mm (HOLD)

SUMP ID: 800mm (HOLD)

**HOLDS:-**  
 1. FLANGES NUMBERS AND SIZE, MECHANICAL TO CONFIRM  
 2. DRUM LOCATION W.R.T. GROUND LEVEL.  
 3. MANWAY LOCATION.

EQUIPMENT NUMBER:	504-V-807
EQUIPMENT NAME:	HOT OIL BLOWDOWN DRUM
PROCESS DATA	
OPERATING TEMPERATURE, °C	100
OPERATING PRESSURE, kg/cm <sup>2</sup> g	1.5
PRELIMINARY MECHANICAL DESIGN DATA	
DESIGN TEMPERATURE, °C	260
DESIGN PRESSURE, kg/cm <sup>2</sup> g	5.0
ASME CODE SECTION VIII:	DIV. 1
INSULATION REQUIRED:	NO
POST-WELD HEAT TREATMENT:	
MATERIALS OF CONSTRUCTION	
	(CORROSION ALLOWANCE (mm)) MATERIAL
SHELL & HEADS:	3 SA516-70 (CS)
PERMANENT INTERNALS:	6 SA516-70 (CS)
REMOVABLE INTERNALS:	3 SA516-70 (CS)

NOZZLE NO.:	NOZZLE TYPES	NUMBER	SIZES (IN)	FLANGE
13	MANWAY	1	24	300HRF
PROCESS NOZZLES:				
1	FEED INLET	1	6	300HRF
11(A/B)	FLANGES	2	24 BY DBE	300HRF
11E	FLANGES	1	24	300HRF
11(C/D)	FLANGES	2	32	300HRF
11F	VENTILATION/FLANGE (NOTE B)	1	8	300HRF
2(A/B)	HOT OIL OUTLET	2	4	300HRF
7(A/B)	TEMPERATURE TAP	2	2	300HRF
8(A/B)	PRESSURE TAP	2	2	300HRF
4	STEAM OUT/N2	1	2	300HRF
9(A-C)	LEVEL TAPS	3	4 BY DBE	300HRF
3	VENTILATION/VENT (NOTE B)	1	8/2	300HRF
5	BEARING COOLING WATER SUPPLY	1	3	300HRF
6	BEARING COOLING WATER RETURN	1	3	300HRF
10	LP FLARE	1	4	300HRF
12	HOT OIL FROM P-813A/B	1	4	300HRF

For Buried vessels (Underground Vessel): Nozzle of size 4" and below shall not be directly mounted on vessels and shall be mounted on a housing nozzle of atleast 8"NB and above. 2 to 4 nos of Nozzles can be combined in a single housing nozzle based on their sizes. External corrosion allowance of minimum 3mm shall be considered in addition to internal corrosion allowance specified in PDS. External stiffeners shall to be provided on all nozzles. All underground vessels shall be anchored with pedestal to resist Buoyancy and anchorage shall be checked against buoyancy. All UG vessels shall be designed for external pressure also considering buried height.




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REVISIONS	
ISSUED FOR REVISED EDP	10-12-18 ALD CLD

SCALE \_\_\_\_\_ DATE \_\_\_\_\_  
 DR. \_\_\_\_\_ CH. \_\_\_\_\_ DR. APP. \_\_\_\_\_ ENGR. \_\_\_\_\_  
 APPROVED: C

**ENGINEERS INDIA LIMITED**  
 (A Govt. of India Undertaking)  
**HINDUSTAN PETROLEUM CORPORATION LTD**  
**VISAKH REFINERY**  
**VISAKH REFINERY MODERNIZATION PROJECT**  
 CLG LC-MAX TECHNOLOGY & ISDTREATING TECHNOLOGY  
 HOT OIL BLOWDOWN DRUM, 504-V-807  
 RESIDUE UPGRADATION FACILITY (RUF)  
 VISAKH REFINERY MODERNIZATION PROJECT (VRMP)  
 HINDUSTAN PETROLEUM CORPORATION LIMITED  
 VISAKHAPATNAM, ANDHRA PRADESH, INDIA  
 BD-175582

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	<b>Residue Upgradation Facility (RUF)</b> <b>EPCC-3 Package for</b> <b>Visakh Refinery Modernization Project (VRMP)</b>	 <i>L&amp;T Hydrocarbon Engineering</i>
		<b>L&amp;T-CHIYODALIMITED</b>
<b>Title: Process Datasheet for HOT OIL BLOWDOWN DRUM (504-V-807)</b> <b>Doc. No.: B016-RUF-LT-504-PC-DS-0288</b>		<b>Rev. No.: 0</b> <b>Page No: 1 of 4</b>



**ANNEXURE – 1****CHANGE LIST**

**General:** This document is based on Licensor datasheet for HOT OIL BLOWDOWN DRUM (504-V-807) issued with bid. Document is further updated based detail engineering requirements (refer Change List below for details).




**Category (C1):** No Change.

**Category (C2):**




Sr. No.	Page No.	Description of change	Reference / Remarks
1.	2	Flanges numbers revised and sizes are defined in nozzle details & corresponding Note 1 is updated.	As per flange design input by Mechanical department. For detail refer mechanical engineering drawing. Number of flanges and detail will be updated in Rev 1 of P&ID: B016-RUF-LT-PID-504-11820.
2.	2	Nozzle numbering is added to nozzle details and on vessel sketch.	For better clarity on nozzle identification. It will be updated in Rev 1 of P&ID: B016-RUF-LT-PID-504-11820.
3.	2	Vent (#3) & steam out nozzles (#4) sizes are confirmed as 2” each as vessel is non-cladded, in nozzle details & corresponding Note 2 is updated.	Reference to EIL BEDB Part B clause 8.5.3.3 (“A758-999-02-41-ODB-1001” pg. 73 of 115).
4.	2	Manway nozzle (#13) size (24”) & location is confirmed & corresponding Note 3 is deleted.	<ol style="list-style-type: none"> <li>1. Location is at top of shell of horizontal vessel. Final location will be decided by Mechanical engineering based on piping. There is no other Process engineering input required.</li> <li>2. Manway size is defined based on EIL BEDB (Part-B) clause 8.5.3.3 A758-999-02-41-ODB-1001 pg. 73 of 115. Missing man-way will be updated in Rev 1 of P&amp;ID: B016-RUF-LT-PID-504-11820.</li> </ol>
5.	2	Drum location w.r.t ground level is defined on	Relative elevation of drum is provided as per piping input considering

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Sr. No.	Page No.	Description of change	Reference / Remarks
		vessel sketch and corresponding Note 4 is modified.	slope of feed inlet header to the vessel.
6.	2	Nozzle (#12) is added for hot oil from pitch solidification area.	To keep it in-line with P&ID: B016-RUF-LT-PID-504-11820 (Rev 0).
7.	2	Feed nozzle (#1) update the location.	The feed nozzle was fouling with knuckle of vessels while placing it above HLL. Hence, the feed nozzle was shifted to shell as marked based on input by Mechanical department.
8.	2	Ventilation/Vent nozzle (#11F) updated to Ventilation/Flange nozzle and Vent nozzle #3 defined separately.	As per mechanical department input, Ventilation nozzle is considered as flange. For further details, please refer Mechanical Engineering Drawing.
9.	2	Cooling water supply and cooling water return word is changed to Bearing cooling water supply (#5) and Bearing cooling water return (#6) respectively in nozzle detail table. Also corresponding changes made in sketch and note 5 i.e. CWS and CWR changed to BCS and BCR.	To keep it in-line with P&ID: B016-RUF-LT-PID-504-11820 (Rev 0).
10.	2	Level tap nozzle (#9A-C) size is defined as 4" for radar type.	As per Instrument design basis & EIL guidelines in doc. no. B016-504-16-EDB-95097-52-0001.
11.	2	Liquid level nomenclature is modified on vessel sketch for better clarity on level identification.	As per EIL guidelines in BEDB (Part-B) Abbreviations on pg. 11 of 115 A758-999-02-41-ODB-1001.
12.	2	High Liquid Level (HLL) is revised from 2200mm to 2100mm. Low liquid level (LLL) is defined as 150 mm.	To place the Feed nozzle above HLL, the HLL was reduced. The total pumpable volume between HLL and LLL is ensured as 40 m <sup>3</sup> as specified in EIL BEDB (Part-B) clause 6.8.2 pg. 44 of 115 A758-999-02-41-ODB-1001. For detail calculations, please refer Annexure 2.

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Sr. No.	Page No.	Description of change	Reference / Remarks
13.	2	Slope is defined as 1% inside vessel and corresponding Note 11 is added.	To drain towards sumps as per good engineering practice. It will be updated in Rev 1 of P&ID: B016-RUF-LT-PID-504-11820.
14.	2	Sump and pump discharge nozzle location is changed in vessel sketch and corresponding Note 11 is added.	Location of sumps is towards sloping end of vessel and minimum from TL. Location is changed in order to ensure complete draining of vessel due to slope.
15.	2	Sanded Packed Note 3 changed to Note 4 in vessel sketch.	To provide correct reference of Note 4.
16.	2	Trim added as Note 9.	As per PMS of inlet and outlet lines indicated in P&ID : B016-RUF-LT-PID-504-11820 (Rev 2)
17.	2	MDMT of 12.5 °C added in Note 10.	As per EIL guidelines in BEDB (Part-B) clause 4.2 pg. 22 of 115 A758-999-02-41-ODB-1001.

	<p style="text-align: center;"><b>Residue Upgradation Facility (RUF)</b> <b>EPCC-3 Package for</b> <b>Visakh Refinery Modernization Project (VRMP)</b></p>	 <i>L&amp;T Hydrocarbon Engineering</i>
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### Liquid level calculations:

#### Basis and assumptions:

As per EIL guidelines in BEDB (Part-B) clause 6.8.2 pg. 44 of 115 A758-999-02-41-ODB-1001, for closed blow-down drum in RUF:

a) Pump-able volume of vessel = 40 m<sup>3</sup>.

b) Pump out flow = 40 m<sup>3</sup>/hr.

As per datasheet,

c) Vessel diameter = 2.5 m

d) Cylindrical length = 8.5 m

#### Conclusions:

1) Volume between LOL & HOL is 32 m<sup>3</sup>.

2) Volume between LLL & HLL is 40 m<sup>3</sup>.

For detail calculations, please refer Annexure 2.

**Project:** Residue Upgradation Facility (RUF) EPCC-3 Package for Visakh Refinery Modernization Project (VRMP).

**ANNEXURE 2**

**Job No.:** B016

**Unit.:** 504

**CHECK FOR LIQUID HOLDUP TIME**

**Vessel Tag No.** 504-V-807

<b>Fluid Flow rate</b>	
Vol. Flow rate	<b>40.0 m3/h</b>

<b>L/D</b>	<b>3.4</b>
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Vessel ID	<b>2.5 m</b>
Cylindrical Length	<b>8.5 m</b>

<b>Volumes, m3</b>	
Head Volume	<b>4.1 Total 45.8</b>
Cylinder Volume	<b>41.7</b>

Level	h	h/d	Cyl. Fraction	angle	cyl vol	Cyl Vol	Head Fraction	Head Vol	Head Vol	Total Vol	Res Time (mins)
LLL	150	0.06	0.349	28.358	1.0	14.55	0.323	0.04	1.321	1.064	2
LOL	300	0.12	0.349	40.536	2.8	14.55	0.323	0.16	1.321	2.998	4
NOL		0	0.500	0.000	0.0	20.86	0.5	0.00	2.045	0.000	-
HOL	1800	0.72	0.349	116.104	32.2	14.55	0.323	3.31	1.321	35.467	53
HLL	2100	0.84	0.651	132.844	37.4	27.18	0.677	3.81	2.769	41.223	62

OPERATING VOL. **32** BETWEEN HOL & LOL  
 OPERATING VOL. **40** BETWEEN HLL & LLL