

	Residue Upgradation Facility (RUF) EPCC-3 Package for Visakh Refinery Modernization Project (VRMP)	 L&T Hydrocarbon Engineering
		L&T-CHIYODA LIMITED
Title: Process Datasheet for AMINE BLOWDOWN DRUM (504-V-804) Doc. No.: B016-RUF-LT-504-PC-DS-0285		Rev. No.: 0 Page No: 1 of 2

OWNER : HINDUSTAN PETROLEUM CORPORATION LIMITED (HPCL)
 PMC : ENGINEERS INDIA LIMITED, NEW DELHI (EIL)
 UNIT : 504
 PMC JOB NO. : B016

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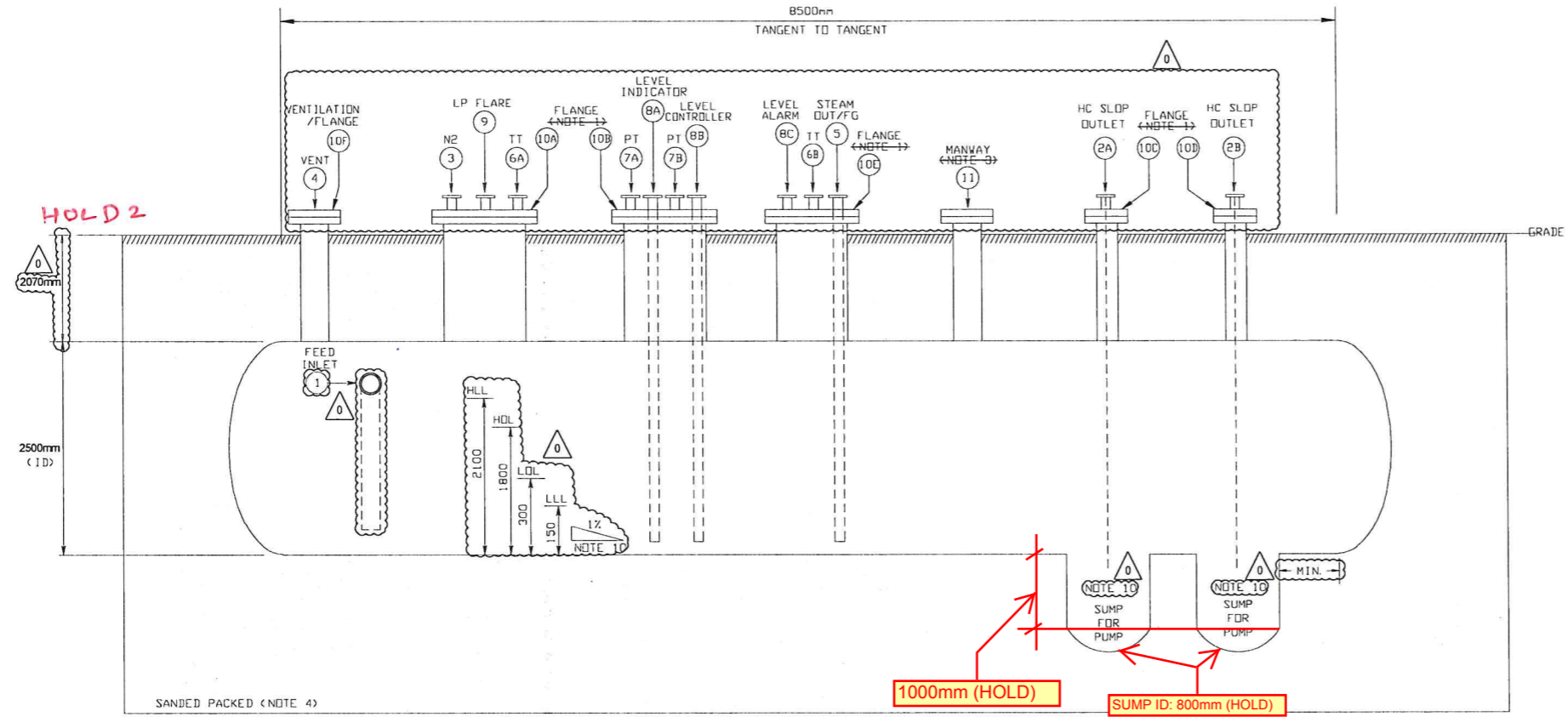
Shell- 28 Thk
 Typical- Head : 2:1 Ellipsoidal Head Thickness : 24 mm Min.
 ALL TOP NOZZLES TYP. PROJECTION FROM VESSEL TOP = 3000 mm (hold)
 FABRICATED WEIGHT = 39000 kg
 PWHT & Impact test requirement : As per code/specification/data sheet
 Note: Above Indicated Weights and Thicknesses for pressure parts and non-pressure parts are minimum to be followed and shall not form the basis for quotation. supplier shall check the thickness to satisfy the requirement of codes ,standards and requisition and guarantee them on strength.

VENDOR TO CONSIDER 5TONS(HOLD) LOAD FOR PUMP FOR PUMP HOSING NOZZLE, THE FINAL LOAD TO BE INFORMED DURING DETAILS ENGINEERING.

100% radiography of all butt joints (longitudinal and circumferential) including nozzle neck to flange, pipe to pipe, pipe to pipe fitting for CS material shall be considered. All CS & LAS parts to be PWHT & hardness of base metal, weld metal and HAZ to be limited as per the Standard Specification.

NOTES
 8. TRIM B94A
 9. MDMT: 12.5°C
 10. VESSEL SHALL BE SLOPED TOWARDS THE SUMP. SUMP SHALL BE LOCATED TOWARDS SLOPING END OF VESSEL.

NOTES
 1. MECHANICAL TO DESIGN ALL FLANGES.
 2. VENT & STEAM OUT NOZZLE SIZES SHOWN ARE BASED ON PROCESS SPECIFICATIONS. ALL BE DR PARTS.
 3. MANWAY SIZE IS RECOMMENDED MINIMUM LOCATION TO BE DETERMINED BY DRG DELETE.
 4. THIS DRUM TO BE LOCATED INSIDE RCC WITH SAND PACKED BY VIBRO COMPRESSION WITH LEAN CONCRETE ON TOP. RELATIVE ELEVATION OF DRUM W.R.T. GROUND LEVEL ETC. TO BE FINALISED BY GENERAL CIVIL BURLING DETAIL ENGINEERING.
 5. STEAM OUT CONDITIONS ARE 0.5 kg/cm²g AND 170°C.
 6. DRUM TO HAVE CATHODIC PROTECTION.
 7. VENTILATION NOZZLE IS TO BE LOCATED TOWARDS THE END OPPOSITE TO THE MANWAY. VENT NOZZLE SHALL BE WELDED TO THE VENTILATION NOZZLE BLIND FLANGE.



EQUIPMENT NUMBER:	504-V-804
EQUIPMENT NAME:	AMINE BLOWDOWN DRUM
PROCESS DATA	
OPERATING TEMPERATURE, °C	56
OPERATING PRESSURE, kg/cm ² g	1.5
PRELIMINARY MECHANICAL DESIGN DATA	
DESIGN TEMPERATURE, °C	260
DESIGN PRESSURE, kg/cm ² g	5.0
ASME CODE SECTION VIII:	DIV. 1
INSULATION REQUIRED:	NO
POST-WELD HEAT TREATMENT:	YES
MATERIALS OF CONSTRUCTION	
(CORROSION ALLOWANCE (mm)) MATERIAL	
SHELL & HEADS:	6 SA516-70 (CS) (NOTE A)
PERMANENT INTERNALS:	6 SA516-70 (CS) OR SA106 GR B (CS)
REMOVABLE INTERNALS:	3 SA516-70 (CS) OR SA106 GR B (CS)
NOTE A: SHALL MEET NACE MRO103 AND PVM-SU-4750 SUPPLEMENT C REQUIREMENTS. SEE GN-9 IN GENERAL NOTES ON MATERIALS OF CONSTRUCTION.	

NOZZLE NO.	NOZZLE TYPES	NUMBER	SIZE(S) (IN)	FLANGE
11	MANWAY	1	24	300HRF
PROCESS NOZZLES:				
1	FEED INLET	1	6	300HRF
10A	FLANGE	1	20 BY DBS	300HRF
10B	FLANGE	1	24	300HRF
10E	FLANGE	1	20	300HRF
10(D/C)	FLANGE	2	32	300HRF
2(A/B)	AMINE SLOP OUTLET	2	4	300HRF
3	NITROGEN	1	2	300HRF
6(A/B)	TEMPERATURE TAP	2	2	300HRF
7(A/B)	PRESSURE TAP	2	2	300HRF
5	STEAM OUT	1	2	300HRF
4	VENT (NOTE 7)	1	2	300HRF
10F	VENTILATION (NOTE 7)	1	8	300HRF
8(A-C)	LEVEL TAPS	3	2	300HRF
9	LP FLARE	1	3	300HRF

HOLDS:-
 1. FLANGES NUMBERS AND SIZE, MECHANICAL TO CONFIRM
 2. DRUM LOCATION w.r.t. GROUND LEVEL
 3. MANWAY LOCATION

For Buried vessels (Underground Vessel): Nozzle of size 4" and below shall not be directly mounted on vessels and shall be mounted on a housing nozzle of atleast 8"NB and above. 2 to 4 nos of Nozzles can be combined in a single housing nozzle based on their sizes. External corrosion allowance of minimum 3mm shall be considered in addition to internal corrosion allowance specified in PDS. External stiffeners shall to be provided on all nozzles. All underground vessels shall be anchored with pedestal to resist Buoyancy and anchorage shall be checked against buoyancy. All UG vessels shall be designed for external pressure also considering buried height.

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ENGINEERS INDIA LIMITED
 HINDUSTAN PETROLEUM CORPORATION LTD
 VISAKH REFINERY
 VISAKH REFINERY MODERNIZATION PROJECT
 CLG LC-MAX TECHNOLOGY & ISDTREATING TECHNOLOGY
 AMINE BLOWDOWN DRUM, 504-V-804
 RESIDUE UPGRADATION FACILITY (RUF)
 VISAKH REFINERY MODERNIZATION PROJECT (VRMP)
 HINDUSTAN PETROLEUM CORPORATION LIMITED
 VISAKHAPATNAM, ANDHRA PRADESH, INDIA

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ANNEXURE – 1**CHANGE LIST**

General: This document is based on Licensor datasheet for AMINE BLOWDOWN DRUM (504-V-804) issued with bid. Document is further updated based detail engineering requirements (refer Change List below for details).




Category (C1): No Change.

Category (C2):




Sr. No.	Page No.	Description of change	Reference / Remarks
1.	2	Flanges numbers revised and sizes are defined in nozzle details & corresponding Note 1 is updated.	As per flange design input by Mechanical department. For detail refer mechanical engineering drawing. Number of flanges and detail will be updated in Rev 1 of P&ID: B016-RUF-LT-PID-504-11813.
2.	2	Vent (#4) & steam out nozzles (#5) sizes are confirmed as 2" each as vessel is non-cladded, in nozzle details & corresponding Note 2 is updated.	As per EIL guidelines in BEDB (Part-B) clause 8.5.3.3 doc. no.: A758-999-02-41-ODB-1001 pg. 73 of 115.
3.	2	Manway nozzle (#11) size (24") and location is confirmed and Note 3 deleted accordingly.	1. Location is at top shell of horizontal vessel. Final location will be decided by Mechanical engineering based on piping. There is no other Process engineering input required. 2. Manway size is defined based on EIL BEDB (Part-B) clause 8.5.3.3 A758-999-02-41-ODB-1001 pg. 73 of 115.
4.	2	Drum location w.r.t ground level is defined on vessel sketch and corresponding Note 4 is modified.	Relative elevation of drum is provided as per piping input considering slope of feed inlet blow down header to the vessel.

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Sr. No.	Page No.	Description of change	Reference / Remarks
5.	2	Nozzle numbering is added to nozzle details and on vessel sketch.	For better clarity on nozzle identification.
6.	2	Feed nozzle (#1) update the location.	The feed nozzle was fouling with knuckle of vessels while placing it above HLL. Hence, the feed nozzle was shifted to shell as marked based on input by Mechanical department.
7.	2	Ventilation/Vent nozzle (#10F) updated to Ventilation/Flange nozzle and Vent nozzle #4 defined separately.	As per mechanical department input, Ventilation nozzle is considered as flange. For further details, please refer Mechanical Engineering Drawing.
8.	2	Level tap nozzle #8 (A-C) size is defined as 4" in nozzle details.	As per Instrument design basis & EIL guidelines in doc. no. B016-504-16-EDB-95097-52-0001.
9.	2	Liquid level nomenclature is modified on vessel sketch for better clarity on level identification.	As per EIL guidelines in BEDB (Part-B) Abbreviations on pg. 11 of 115 A758-999-02-41-ODB-1001.
10.	2	High Liquid Level (HLL) is revised from 2200mm to 2100mm. Low liquid level (LLL) is defined as 150 mm.	To place the Feed nozzle above HLL, the HLL was reduced. The total pumpable volume between HLL and LLL is ensured as 40 m ³ as specified in EIL BEDB (Part-B) clause 6.8.2 pg. 44 of 115 A758-999-02-41-ODB-1001. For detail calculations, please refer Annexure 2.
11.	2	Slope is defined as 1% inside vessel and corresponding Note 10 is added.	To drain towards sumps as per good engineering practice. It will be updated in Rev 1 of P&ID: B016-RUF-LT-PID-504-11813.
12.	2	Sump and pump discharge nozzle location is changed in vessel sketch and corresponding Note 10 is added.	Location of sumps is towards sloping end of vessel and minimum from TL. Location is changed in order to ensure complete draining of vessel due to slope.
13.	2	Sanded Packed Note 3 changed to Note 4 in vessel sketch.	To provide correct reference of Note 4.

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Sr. No.	Page No.	Description of change	Reference / Remarks
14.	2	Trim added as Note 8.	As per PMS of inlet and outlet lines indicated in P&ID : B016-RUF-LT-PID-504-11813 Rev 0.
15.	2	MDMT of 12.5 °C added in Note 9.	As per EIL guidelines in BEDB (Part-B) clause 4.2 pg. 22 of 115 A758-999-02-41-ODB-1001.

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Liquid level calculations:

Basis and assumptions:

As per EIL guidelines in BEDB (Part-B) clause 6.8.2 pg. 44 of 115 A758-999-02-41-ODB-1001, for closed blow-down drum in RUF:

- a) Pump-able volume of vessel = 40 m³.
- b) Pump out flow = 40 m³/hr.

As per datasheet,

- c) Vessel diameter = 2.5 m
- d) Cylindrical length = 8.5 m

Conclusions:

- 1) Volume between LOL & HOL is 32 m³.
- 2) Volume between LLL & HLL is 40 m³.

For detail calculations, please refer Annexure 2.

Project: Residue Upgradation Facility (RUF) EPCC-3 Package for Visakh Refinery Modernization Project (VRMP).

ANNEXURE 2

Job No.: B016

Unit.: 504

CHECK FOR LIQUID HOLDUP TIME

Vessel Tag No. 504-V-804

Fluid Flow rate	
Vol. Flow rate	40.0 m3/h

L/D	3.4
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Vessel ID	2.5 m
Cylindrical Length	8.5 m

Volumes, m3	
Head Volume	4.1 Total 45.8
Cylinder Volume	41.7

Level	h	h/d	Cyl. Fraction	angle	cyl vol	Cyl Vol	Head Fraction	Head Vol	Head Vol	Total Vol	Res Time (mins)
LLL	150	0.06	0.349	28.358	1.0	14.55	0.323	0.04	1.321	1.064	2
LOL	300	0.12	0.349	40.536	2.8	14.55	0.323	0.16	1.321	2.998	4
NOL		0	0.500	0.000	0.0	20.86	0.5	0.00	2.045	0.000	-
HOL	1800	0.72	0.349	116.104	32.2	14.55	0.323	3.31	1.321	35.467	53
HLL	2100	0.84	0.651	132.844	37.4	27.18	0.677	3.81	2.769	41.223	62

OPERATING VOL. **32** BETWEEN HOL & LOL
 OPERATING VOL. **40** BETWEEN HLL & LLL